

شركة الخليج لصناعة البتروكيماويات  
Gulf Petrochemical Industries Company  
Kingdom of Bahrain



Carbon Dioxide Recovery (CDR) Project

# Introduction

Established in December 1979

Joint-Venture between the Government of Bahrain , SABIC & PIC

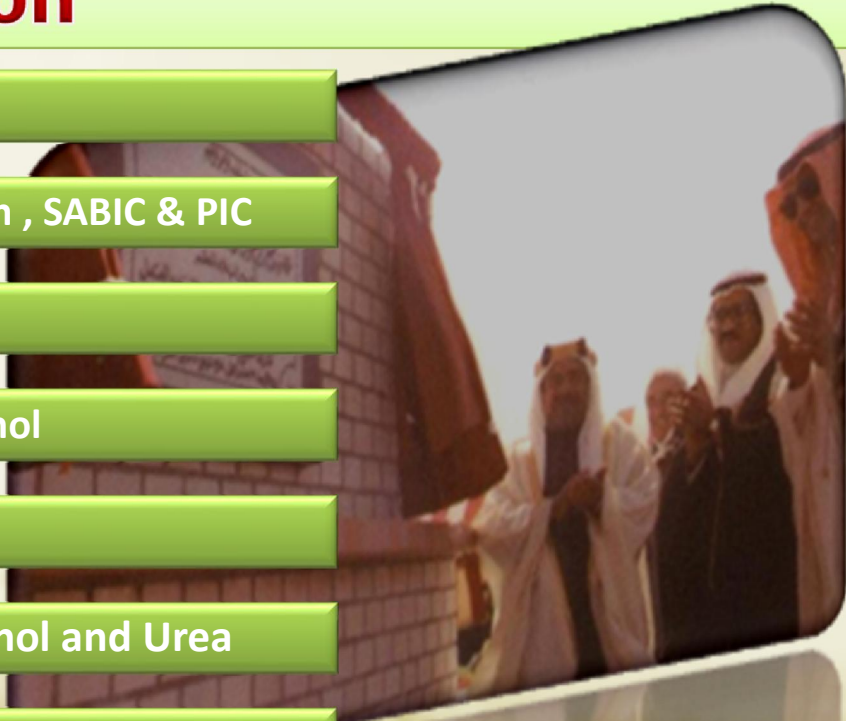
Utilizes Natural Gas as raw material

Started production in 1985 : Ammonia , Methanol

Started Urea Production in 1998

Started production in 1985 : Ammonia , Methanol and Urea

MHI CDR plant commissioned in 2009





## Our Mission

To add value to our customers and shareholders by meeting their expectations whilst:

Producing high quality products

Focusing on customers

Optimising business in a cost effective, safe, environmentally friendly and socially responsible way

Embracing knowledge, creativity and best practices

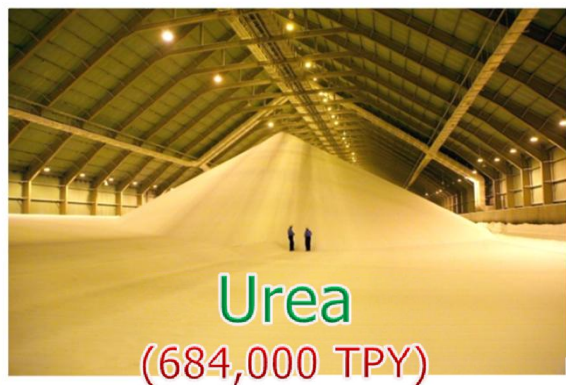
## Our Vision

To be a global, dynamic world-class petrochemical and fertilizer company of choice recognized for excellence.

# GPIC Mission & Vision

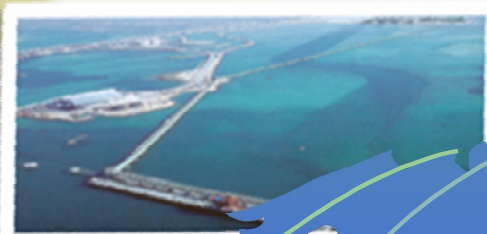
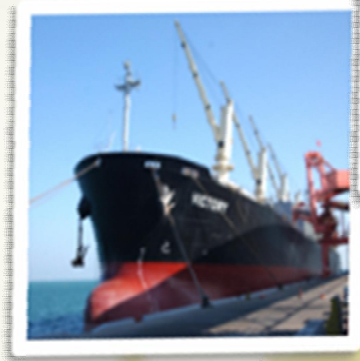


# Total Production

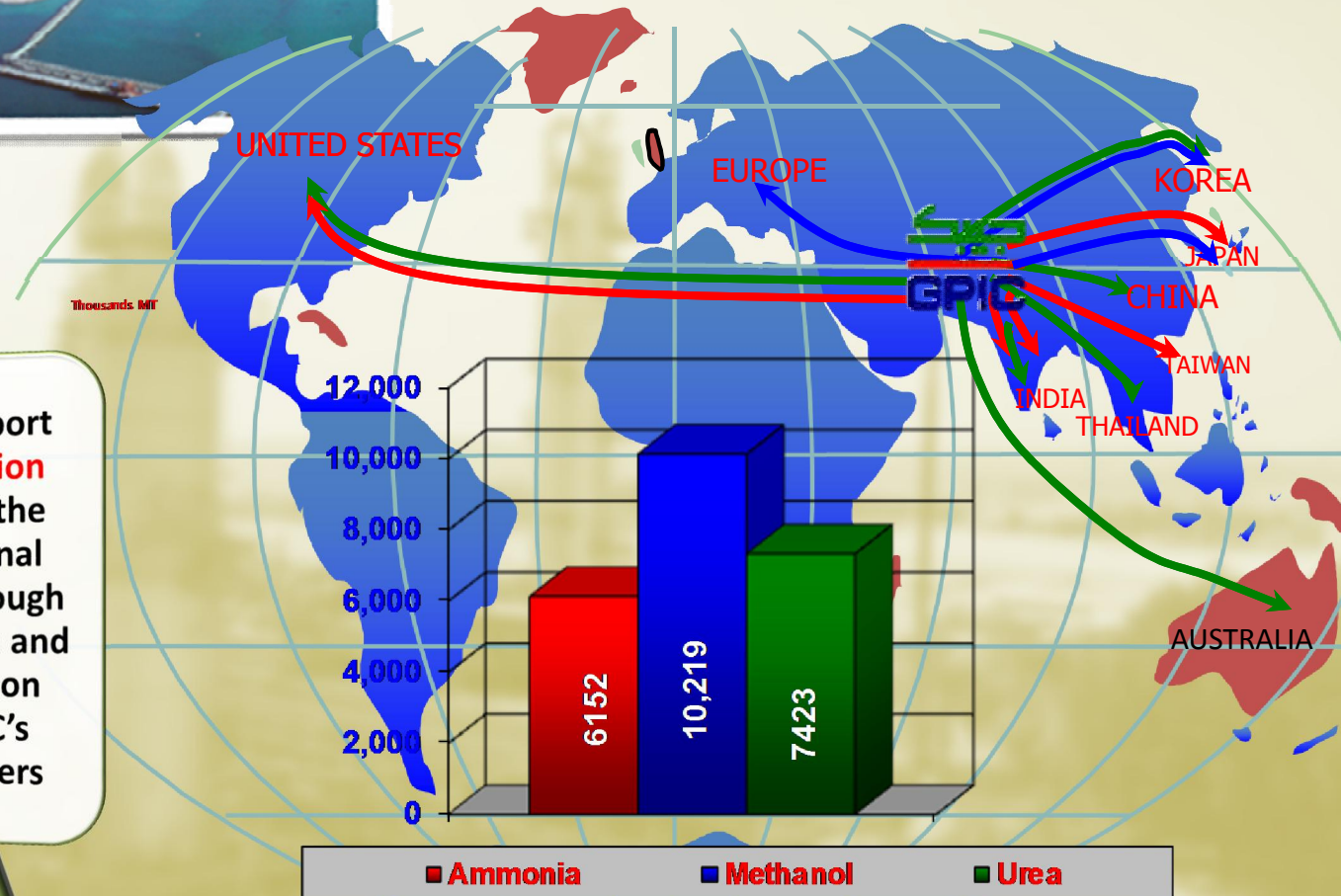




# Marketing & Export



Annual export of **1.2 Million tonnes** to the International Market through cooperation and coordination with GPIC's Shareholders



# Objectives of the CDR Project



## Objective of CDR Project



### Preserve Environment

Reduce the emission of green house gases

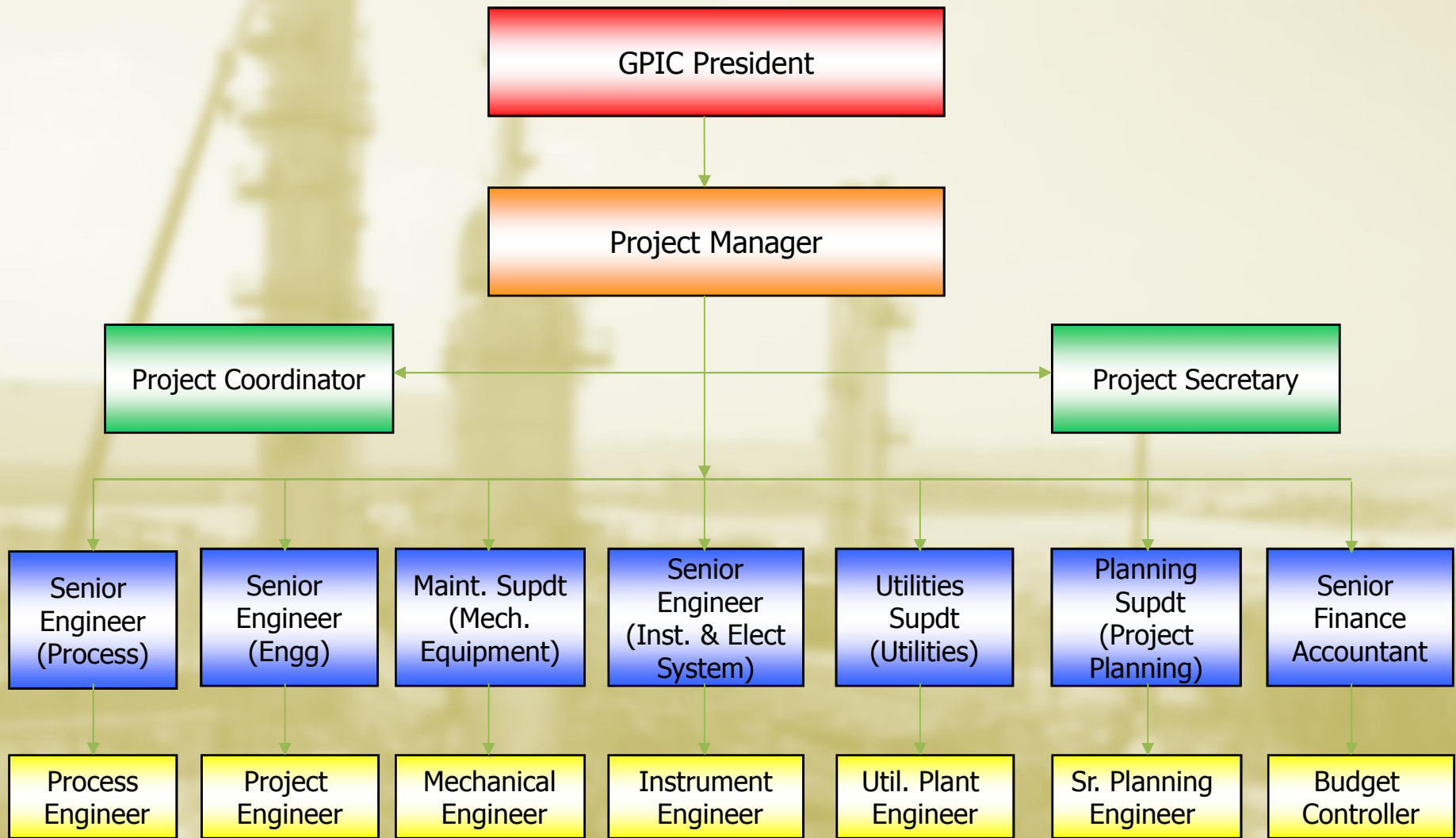
Recovery of 148,500 MT per annum of CO<sub>2</sub>

### Increase Production

Urea production by ~ 26,400 MT per annum

Methanol production by ~ 39,600 MT per annum

# Project Organization Chart





# Project Materialization

## CDR Project Feasibility Study

- Explore the market and price outlook for both Methanol and Urea in the medium and long term
- Explore technology options and project cost
- Assess the economics (e.g. ROI, IRR)

# Strategic outlines during Project conceptualization

GPIC strategic outlines were in terms of....

- Selection criteria for the CDR plant Capacity
- Selection criteria for the Technology
- Selection criteria for the EPC Contractor

# Selection criteria for the CDR plant Capacity

- Proven production capacity
- Capacity similar to regional and international practice
- Capacity compatible with GPIC raw materials (i.e. similar flue gases) and space availability for the Project

450 MTPD capacity of CDR Plant



# Selection Criteria for the Technology

- Proven technology
- Reliable in terms of operation and maintenance
- Positive Environmental impact

MHI's CDR technology

# Selection criteria for the EPC Contractor

- Contractor with relevant experience
- Contractor with proven records (financially and operationally)
- Competitive offer

Technimont ICB  
(Italian-Indian joint venture Company)

# Project Commencement

## Compilation of ITB

CDR team compiled the Specs, standards and Scope of Works and all the requirements identified during the conceptualization and planning phases of the Project in the ITB.



# Requirements During Project Planning Phase

- Maximum involvement of GPIC's operation, maintenance, engineering, and finance since inception of the Project.
- EPC Contractor to accommodate operation, maintenance and training requirements during the basic and detailed engineering phases.
- GPIC's approval is a "must" for Vendors and Subcontractors selection.

# Requirements During Project Planning Phase

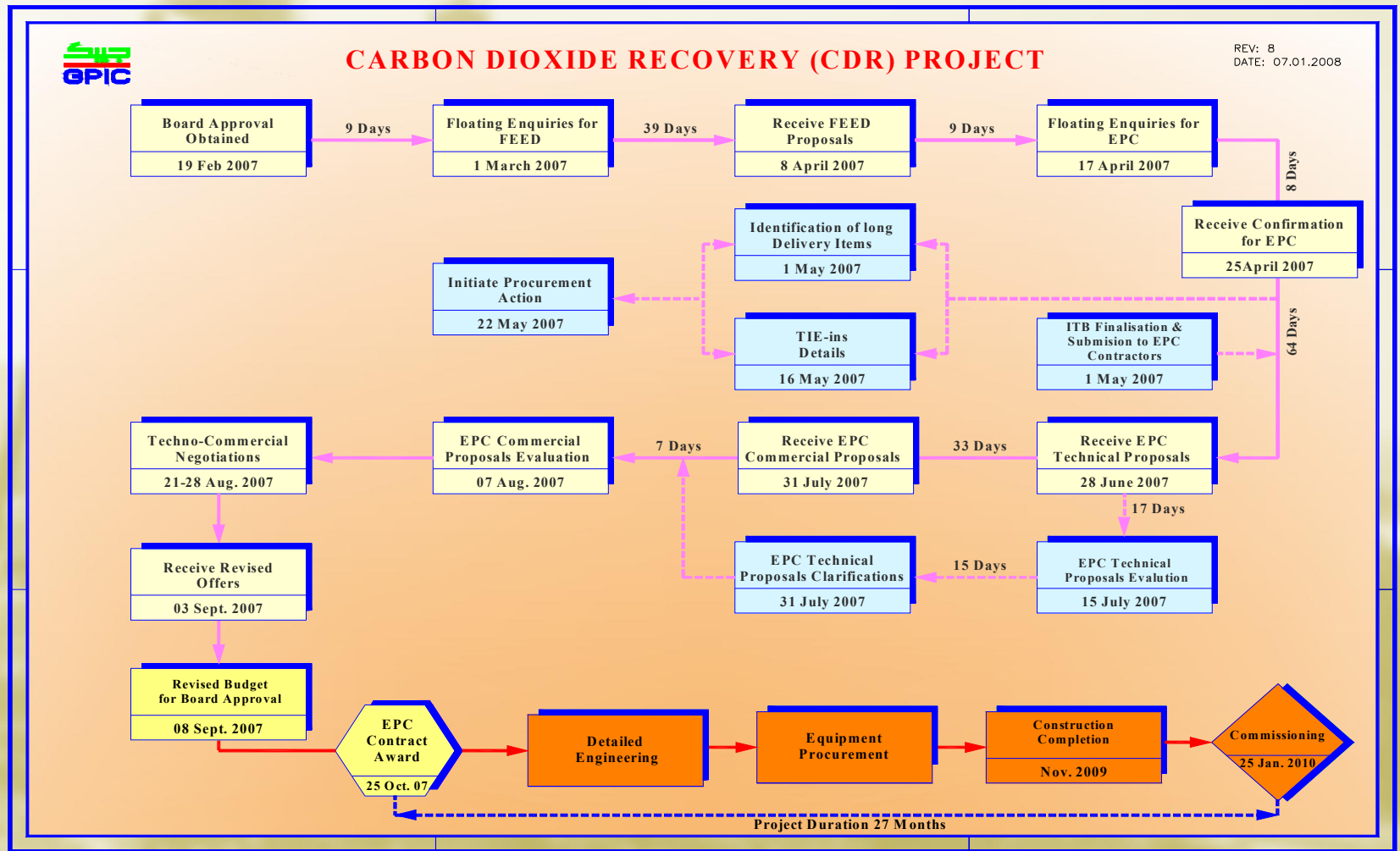
- Visits to be arranged to similar operating plants to learn from their experience
- Project Management shall be through GPIC project team
- Synergy and Integration study with the existing plant to be carried out
- Third party inspection of critical equipment
- Commissioning of the plant shall be by the owner's personnel, under the supervision of the EPC Contractor

# Requirements During Project Planning Phase

- Use of effective Planning and Scheduling tools.
- HAZOP review should be carried out during development, engineering and implementation of the Project.
- Pre Start-up Safety Review and Hazard study at the end of the construction stage prior to start up
- Carry out the Environment Impact Assessment & Business Risk Assessment for the Project.



# CDR Project Road Map



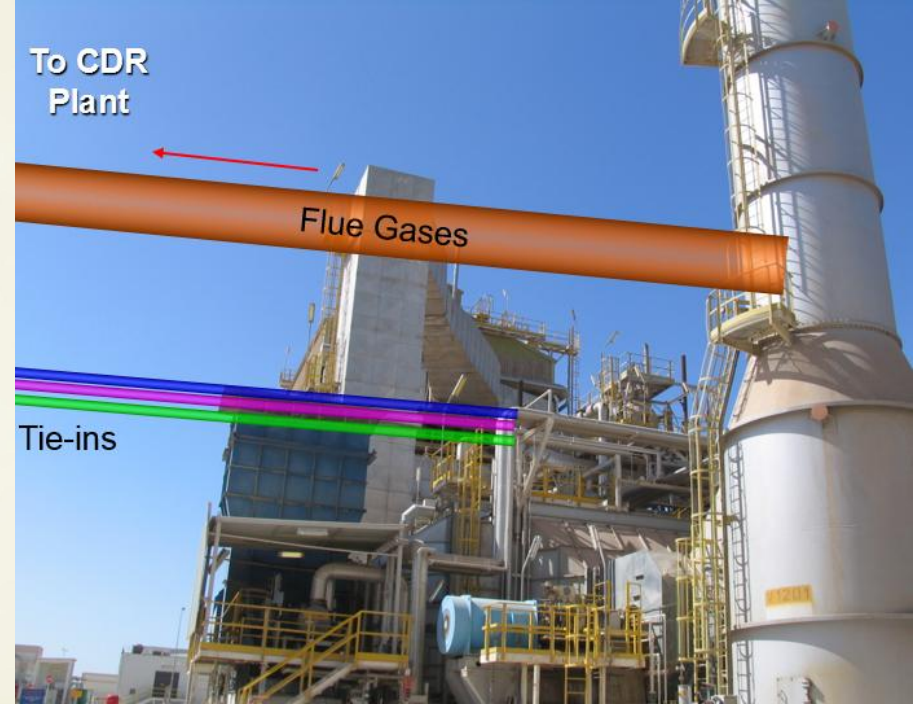
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# CDR Milestones

Activity	Date
CDR Agreement Signing	25 <sup>th</sup> October 2007
KS1 Solution Agreement Signing	4 <sup>th</sup> April 2008
Construction Works Commencement	1 <sup>st</sup> June 2008
Inauguration by GPIC MD	27 <sup>th</sup> August 2008
Electrical Works Completion	25 <sup>th</sup> November 2009
Mechanical Completion	25 <sup>th</sup> November 2009
Instrument Works Completion	3 <sup>rd</sup> December 2009
Boiler Commissioning	5 <sup>th</sup> December 2009
CO <sub>2</sub> Production	20 <sup>th</sup> December 2009

# List of tie-ins

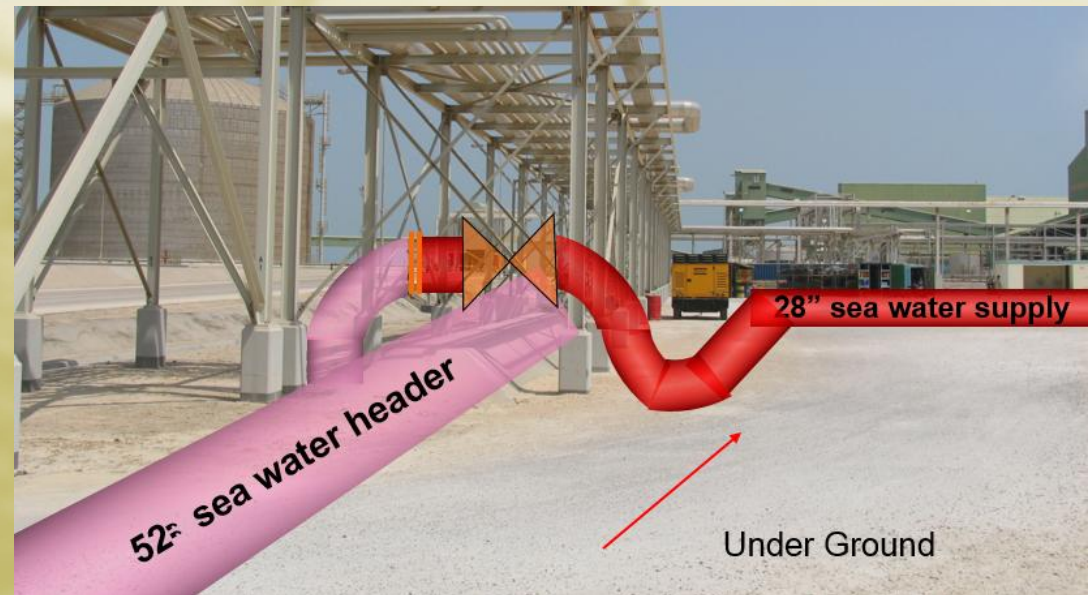
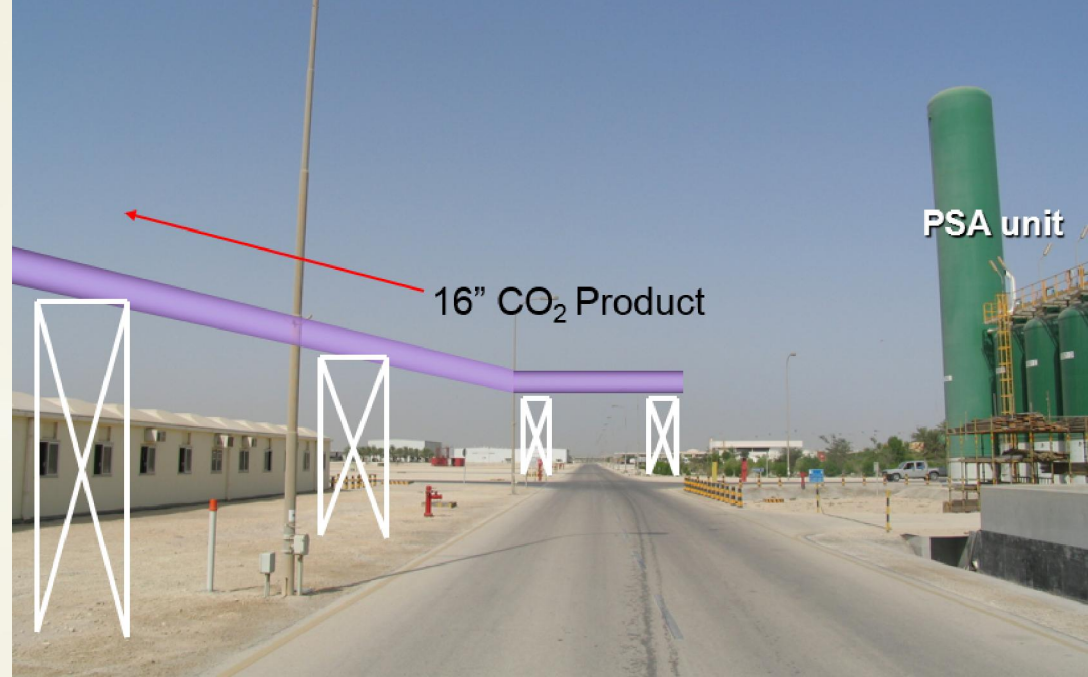
- Flue gas (at reformer stack)
- Service water
- Product CO<sub>2</sub> (at urea B/L)
- Natural gas
- SW supply / return
- FCW supply / return
- LH steam
- Potable water
- Nitrogen





# List of tie-ins

- Plant air
- Instrument control power
- Electric power
- DM water
- Fire water
- Instrument air
- Steam condensate



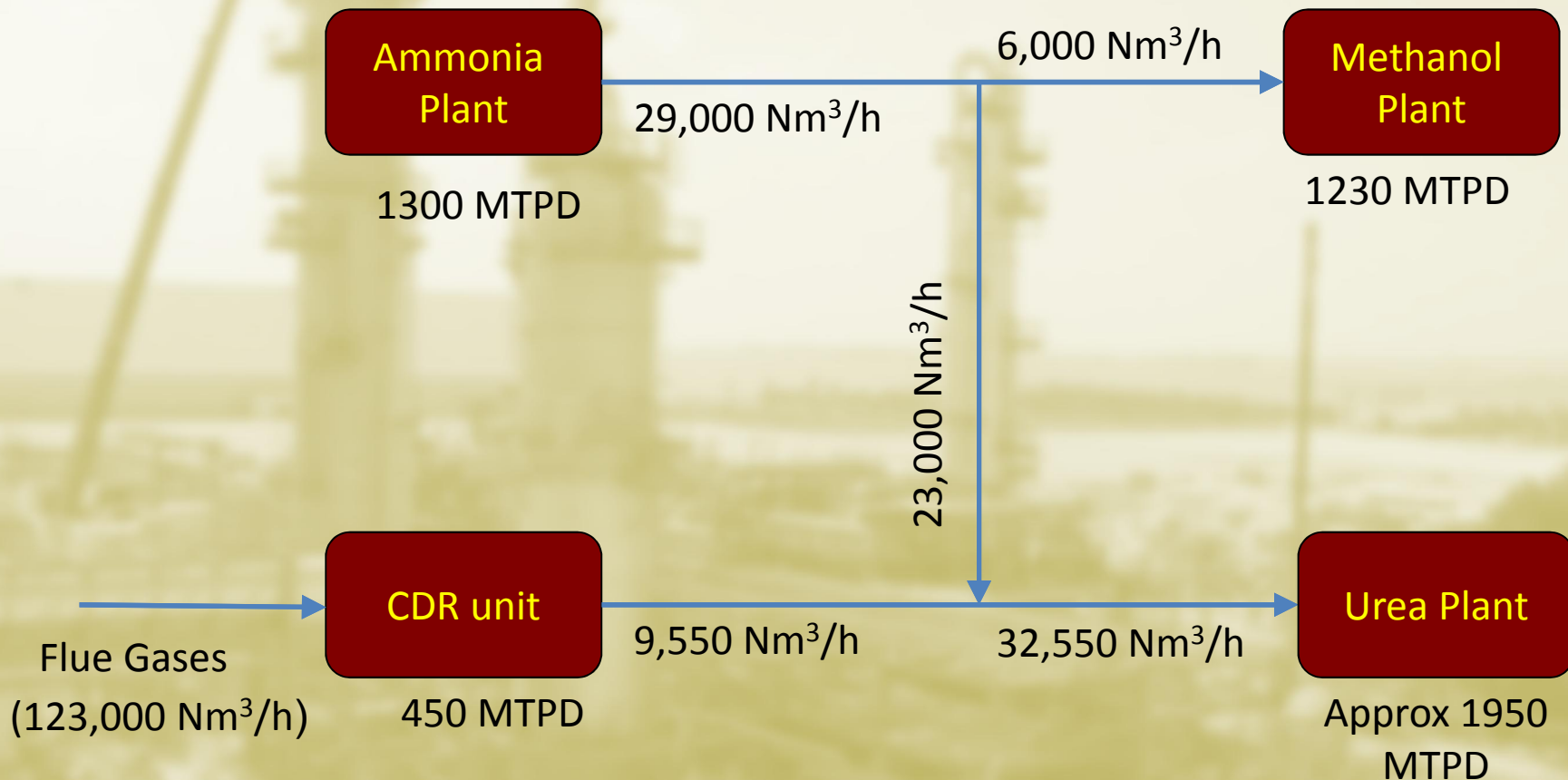
# Technical Features of MHI's Technology

MHI's flue gas CO<sub>2</sub> capturing technology uses a solvent which is patented as KS-1, an amine based solvent.

Following are the main features :

- Solvent has high loading rate
- Low residual CO<sub>2</sub> in the lean solvent, overall recovery process efficient
- KS-1 solvent not very corrosive
- Formation of heat stable salts – minimum
- Frequency of reclamation – very low
- Incinerator required to dispose off the degraded solvent.

# CO<sub>2</sub> Gas Balance after CDR





# CDR Safety

ONE Million man hours worked  
without LTA

Safety procedures

Daily toolbox talks

Emergency procedures

Frequent safety audits

Designated safety watch

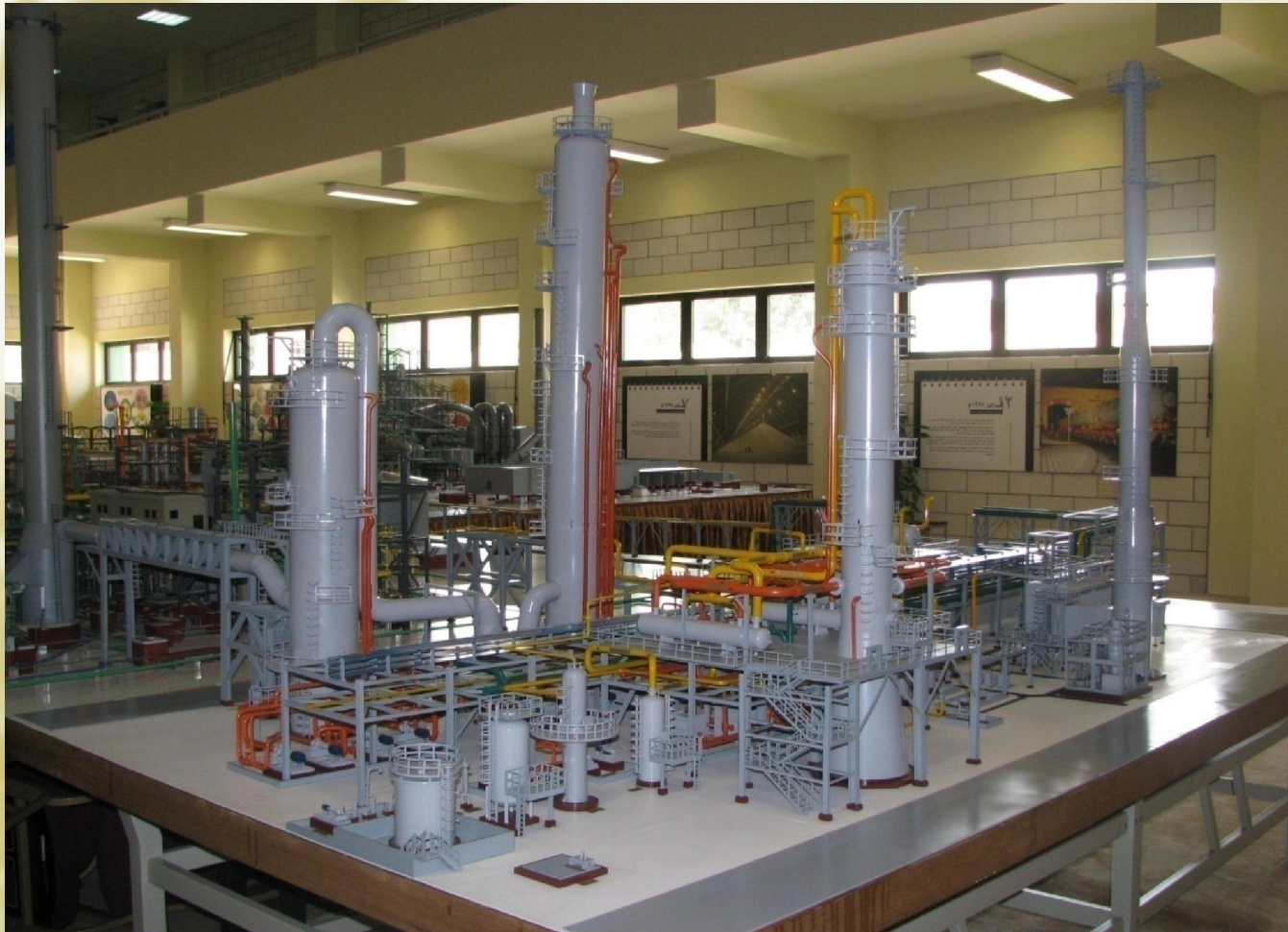
# CDR Benefits

- GPIC urea and methanol production increased by 200 MTPD.
- The specific energy consumption per ton of Methanol and Urea has reduced post CDR operation.



# CDR Photos

CDR Model





# CDR Photos



**CDR Construction Site Aerial View**



# CDR Photos



# CDR Photos









# Thank You